

Major Test – CHL604

Answer all questions

1. For the reduction of Fe_3O_4 to metallic iron by H_2 gas, determine the time required for 50% penetration of the reaction front assuming shrinking core model. Data is

$$\rho_s = 4.6 \text{ gm/cc, M.W of Fe} = 56$$

$$E = 24000 \text{ cal/mol, } A = 1.93 \times 10^5 \text{ cm/s}$$

$$P = 1 \text{ atm } T = 600^\circ\text{C}$$

2. A solid feed consisting of the distribution of particles as

$$d_p \rightarrow 1\text{mm } 2\text{mm } 4\text{mm}$$

$$\text{Wt\%} \rightarrow 20 \quad 30 \quad 50$$

is passed through a tubular reactor where it reacts with a gas to form solid product. Assume the reaction to be chemical reaction control according to shrinking core model. The time for complete conversion of 4 mm particles is 4 hrs. Find the residence time required for 75% conversion of the solid feed.

3. For a catalytic gas-reaction $A \rightleftharpoons B$, derive the overall rate equation for adsorption of A as rate controlling. (Neglect gas-film, diffusional resistances).
4. What is independent deactivation of a catalyst? Derive an equation for the activity of the catalyst for the above case.

The following data is obtained for an irreversible reaction with a decaying catalyst in a batch reactor with batch catalyst and gas. Determine the Kinetics.

$$C_A = 1.0 \quad 0.802 \quad 0.675 \quad 0.532 \quad 0.422 \quad 0.368$$

$$t(\text{hr}) = 0 \quad 0.25 \quad 0.5 \quad 1.0 \quad 2.0 \quad \infty$$

5. The reaction $A \rightarrow 4R$ is carried out in a tubular packed catalyst bed reactor. Determine the wt of the catalyst required for 35% conversion of A. Pure A enters the reactor at 117°C , 3.2 atm pressure and 1000 moles/hr. The rate constant is $9.6 \times 10^{-3} \text{ m}^3/\text{hr. Kg cat.}$ Show the derivation of the required equation separately.
6. For a packed bed catalytic reactor, derive the governing equation with B.C. conditions and transform into dimensionless form also. Assume isothermal condition and no radial mass transfer.